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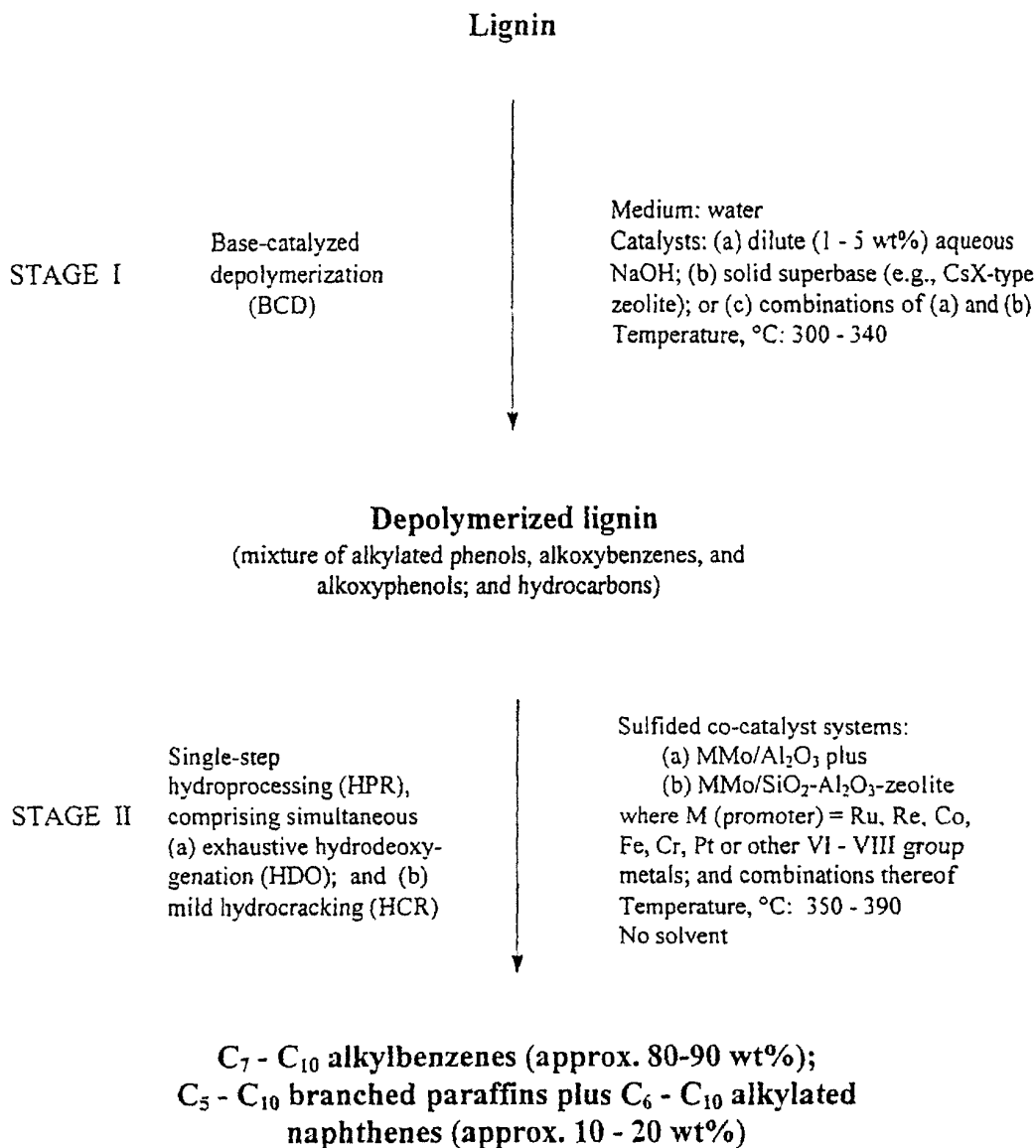


Figure 1a Schematic flow diagram of the two-stage (BCD-HPR) process for conversion of lignin to C<sub>7</sub> - C<sub>10</sub> alkylbenzenes as gasoline blending components according to the present invention.

# Process Concept for Converting Lignin into High-Octane Fuel Additive

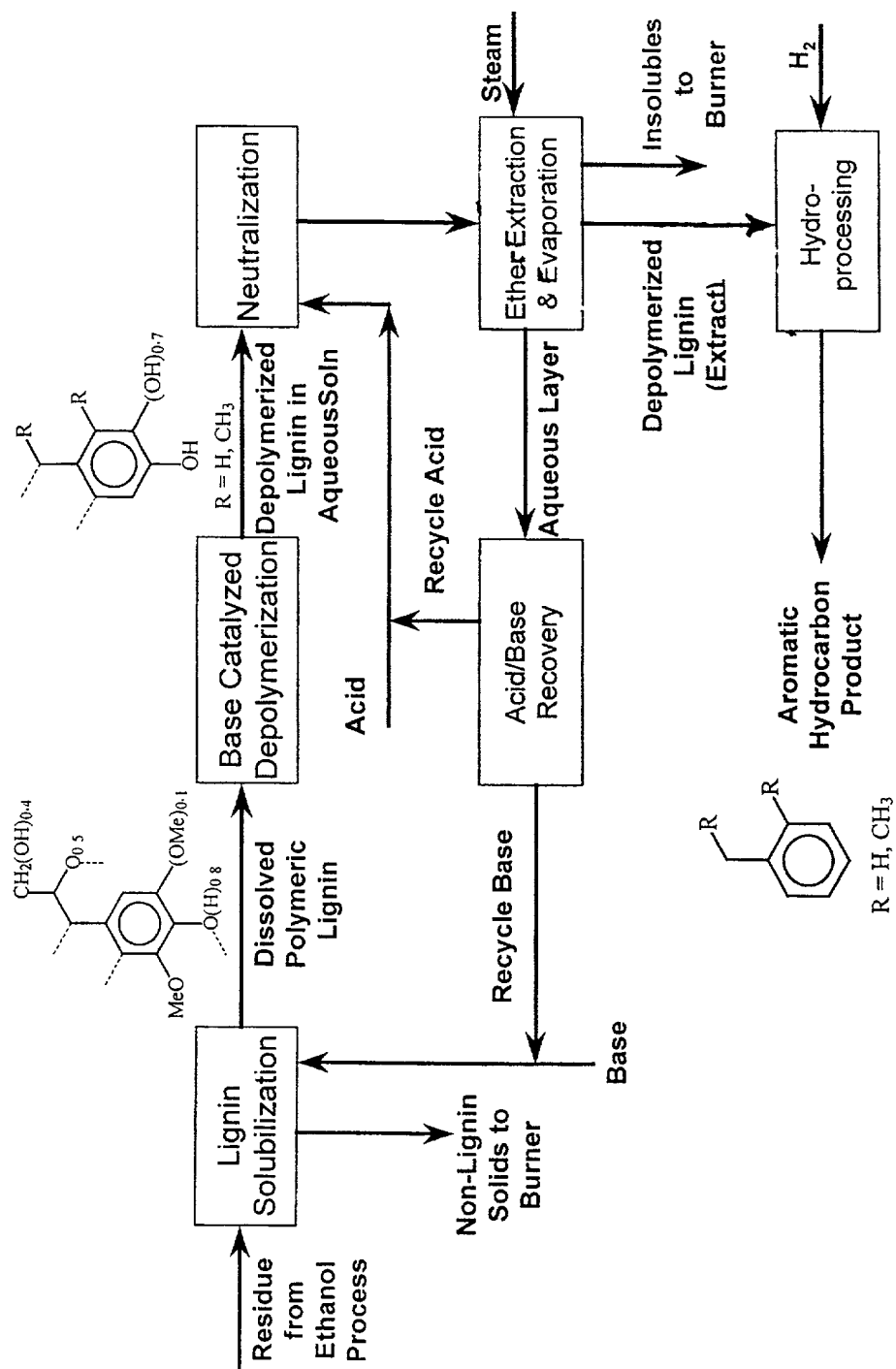


Figure 1b

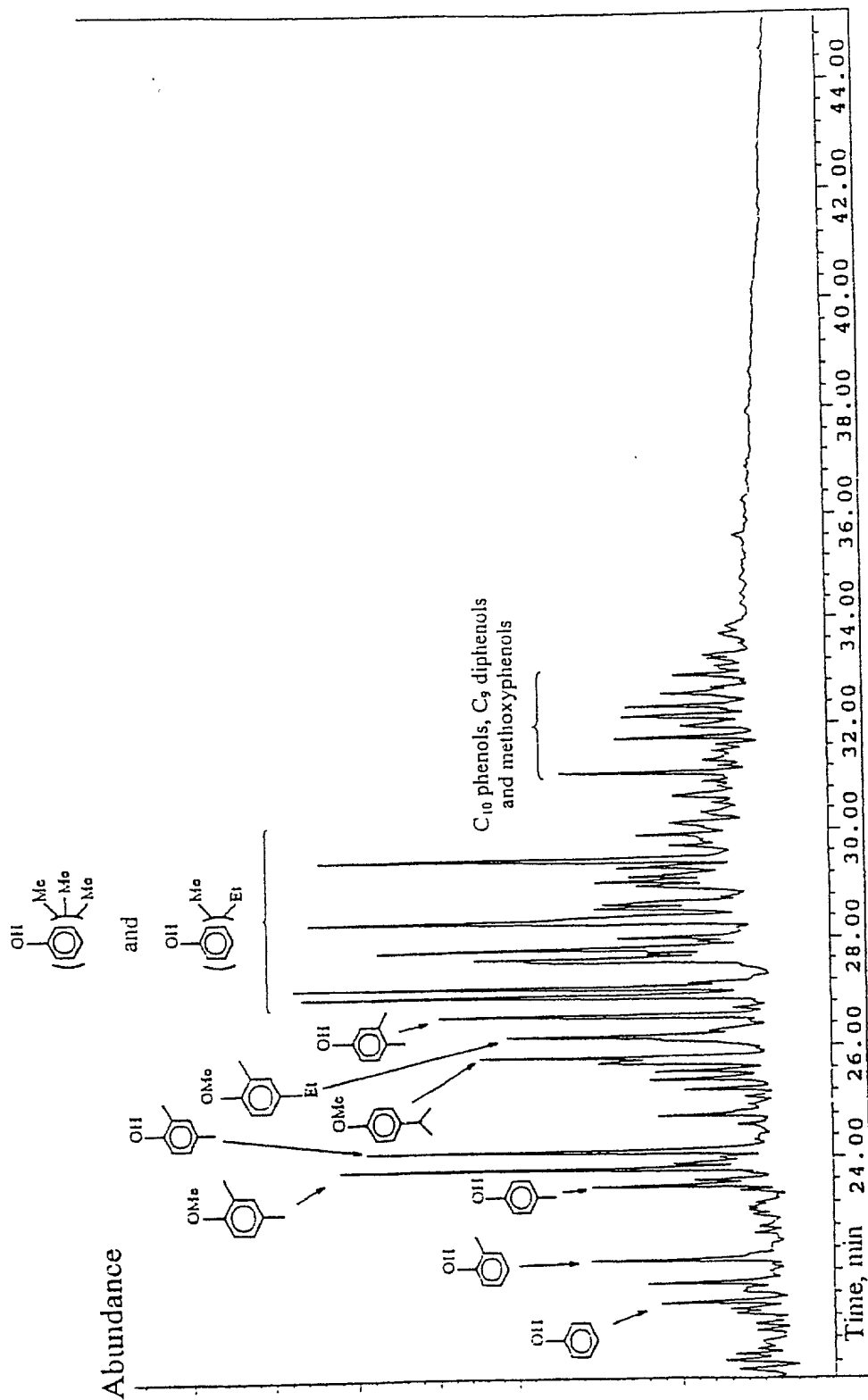


Figure 2. Example of GC/MS analysis of depolymerized (BCD) product from Repap lignin.

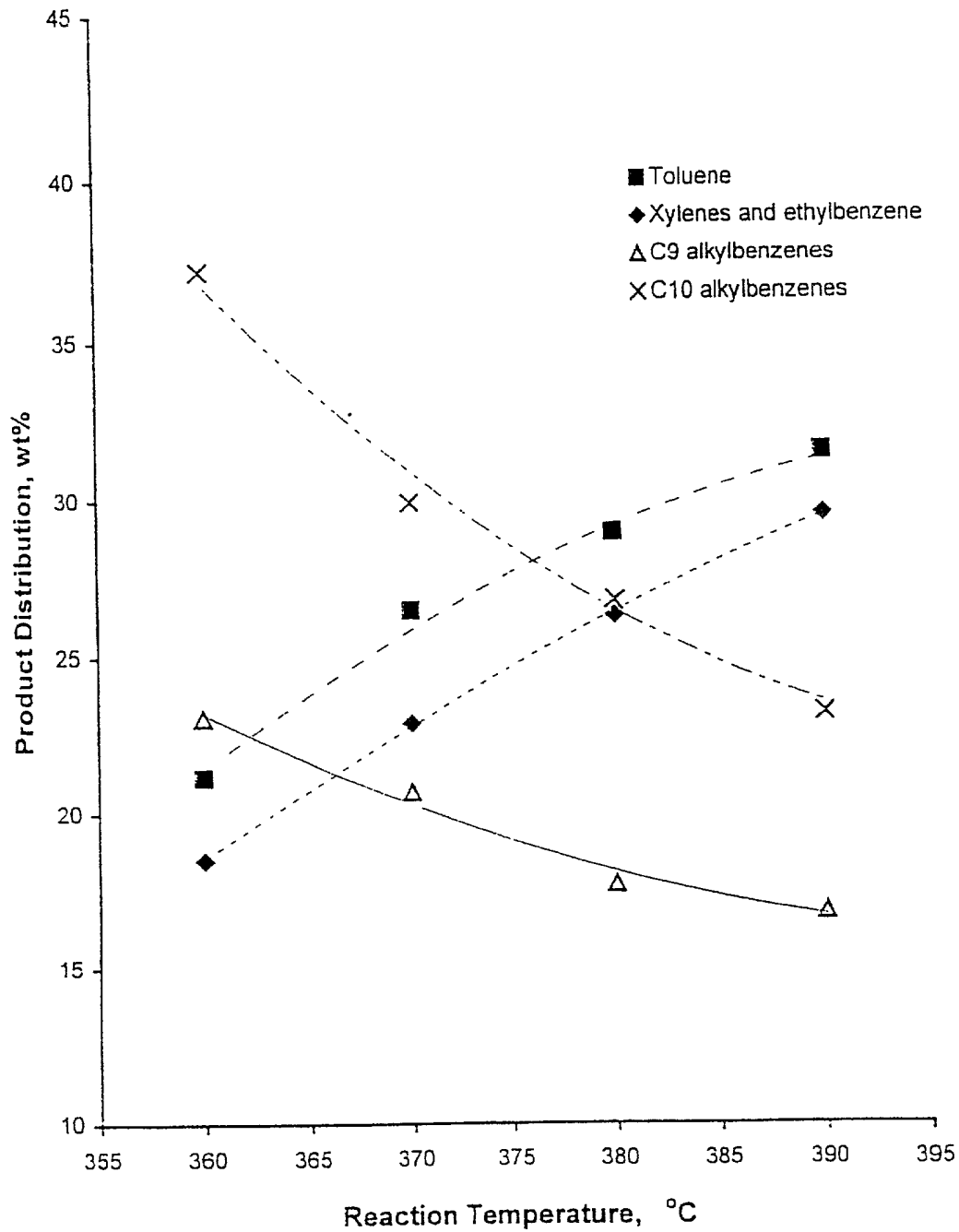


Figure 3. Change in Composition of C<sub>7</sub> - C<sub>10</sub> Alkylbenzene Products from BCD-HPR of Repap Lignin, as a Function of HPR Reaction Temperature

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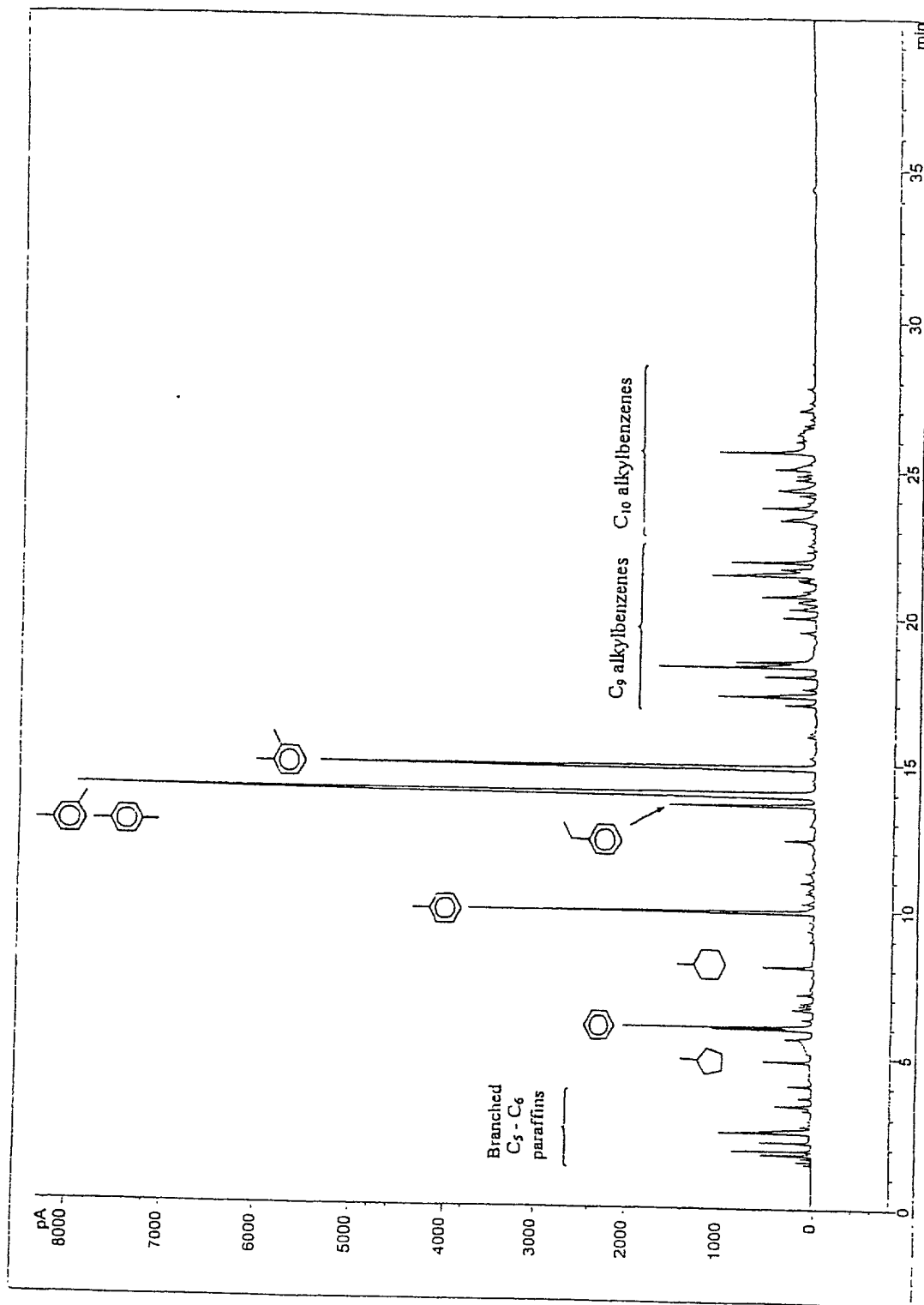


Figure 4. Example of GC/MS analysis of HPR product from depolymerized Repap lignin (HPR temperature, 380 °C; H<sub>2</sub> pressure, 500 psig; LHSV = 4 h<sup>-1</sup>; HCR/HDO co-catalyst wt. ratio, 1 : 9).

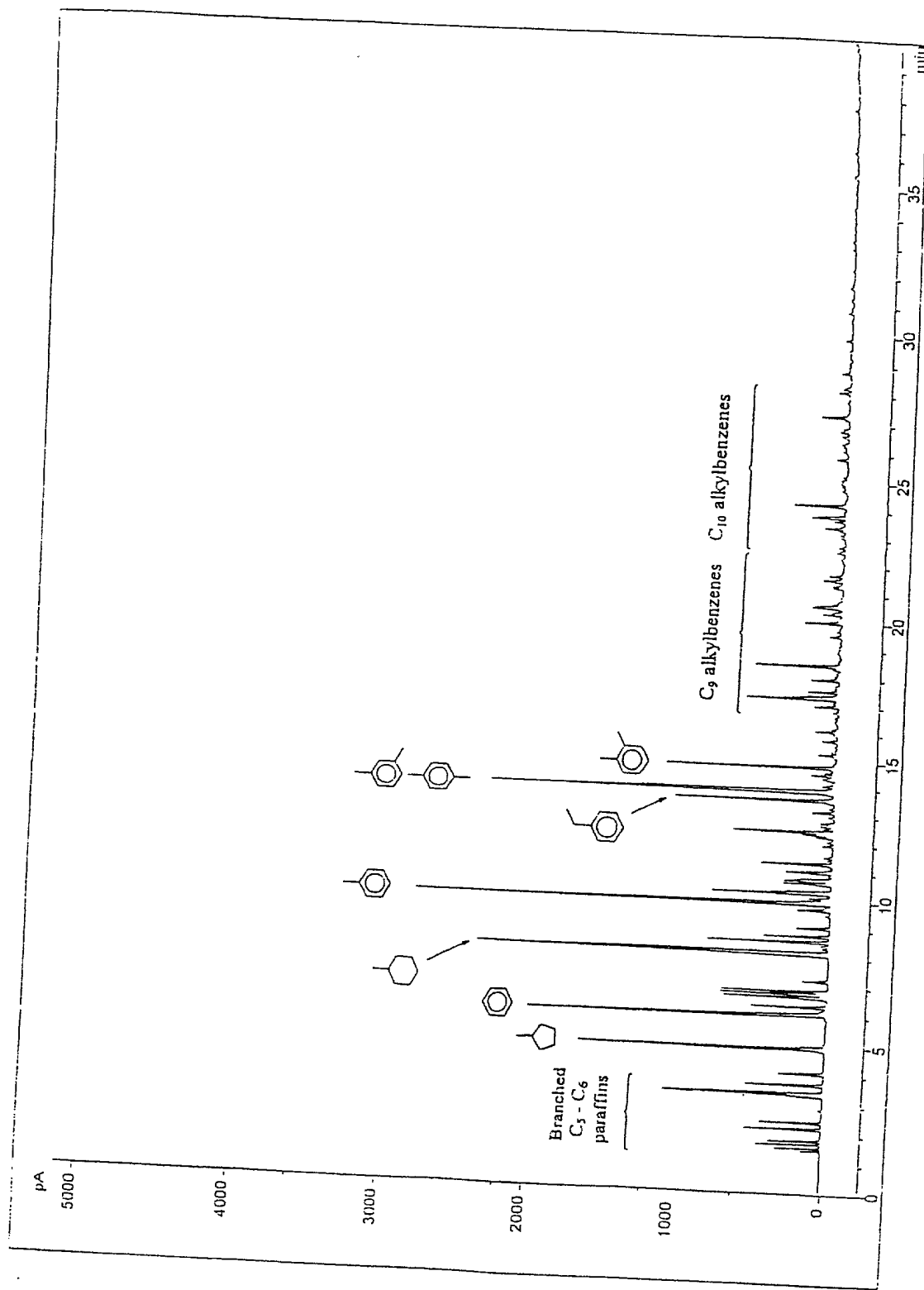


Figure 5. Example of GC/MS analysis of HPR product from depolymerized Repap lignin (HPR temperature, 380 °C; I<sub>2</sub> pressure, 1500 psig; LHSV = 4 h<sup>-1</sup>; HCR/HDO co-catalyst wt. ratio, 1 : 4).